



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : C08G 67/00, 85/00, C08J 3/28, C08F 2/48, 4/28, 10/00, 10/02, 10/04, 10/06, 10/08, 10/10, 10/14, 14/18, 14/24, 14/26, 14/28	A1	(11) International Publication Number: WO 97/28205 (43) International Publication Date: 7 August 1997 (07.08.97)
(21) International Application Number: PCT/US97/01518 (22) International Filing Date: 29 January 1997 (29.01.97) (30) Priority Data: 08/593,838 30 January 1996 (30.01.96) US (60) Parent Application or Grant (63) Related by Continuation US 08/593,838 (CON) Filed on 30 January 1996 (30.01.96) (71) Applicant (for all designated States except US): THE UNIVERSITY OF NORTH CAROLINA AT CHAPEL HILL [US/US]; 300 Bynum Hall, Chapel Hill, NC 27599 (US). (72) Inventors; and (75) Inventors/Applicants (for US only): DeSIMONE, Joseph, M. [US/US]; 2002 Pathway Drive, Chapel Hill, NC 27516 (US). ROMACK, Timothy, J. [US/US]; 5810 Forest Ridge Drive, Durham, NC 27713 (US).	(74) Agents: SIBLEY, Kenneth, D. et al.; Bell, Seltzer, Park & Gibson, P.O. Drawer 34009, Charlotte, NC 28234 (US). (81) Designated States: AL, AM, AT, AT (Utility model), AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, CZ (Utility model), DE, DE (Utility model), DK, DK (Utility model), EE, EE (Utility model), ES, FI, FI (Utility model), GB, GE, HU, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SK (Utility model), TJ, TM, TR, TT, UA, UG, US, UZ, VN, ARIPO patent (KE, LS, MW, SD, SZ, UG), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG). Published <i>With international search report.</i>	
(54) Title: METHOD FOR OLEFIN OXIDATION (57) Abstract <p>A process for making oxidized olefins is disclosed. Specifically, the process comprises providing an olefin and oxygen in combination in a reaction medium comprising carbon dioxide, and then oxidizing the olefin in the reaction medium to make the oxidized olefin. Preferably, a perfluoropolyether is produced by the process.</p>		

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AM	Armenia	GB	United Kingdom	MW	Malawi
AT	Austria	GE	Georgia	MX	Mexico
AU	Australia	GN	Guinea	NE	Niger
BB	Barbados	GR	Greece	NL	Netherlands
BE	Belgium	HU	Hungary	NO	Norway
BF	Burkina Faso	IE	Ireland	NZ	New Zealand
BG	Bulgaria	IT	Italy	PL	Poland
BJ	Benin	JP	Japan	PT	Portugal
BR	Brazil	KE	Kenya	RO	Romania
BY	Belarus	KG	Kyrgyzstan	RU	Russian Federation
CA	Canada	KP	Democratic People's Republic of Korea	SD	Sudan
CF	Central African Republic	KR	Republic of Korea	SE	Sweden
CG	Congo	KZ	Kazakhstan	SG	Singapore
CH	Switzerland	LJ	Liechtenstein	SI	Slovenia
CI	Côte d'Ivoire	LK	Sri Lanka	SK	Slovakia
CM	Cameroon	LR	Liberia	SN	Senegal
CN	China	LT	Lithuania	SZ	Swaziland
CS	Czechoslovakia	LU	Luxembourg	TD	Chad
CZ	Czech Republic	LV	Latvia	TG	Togo
DE	Germany	MC	Monaco	TJ	Tajikistan
DK	Denmark	MD	Republic of Moldova	TT	Trinidad and Tobago
EE	Estonia	MG	Madagascar	UA	Ukraine
ES	Spain	ML	Mali	UG	Uganda
FI	Finland	MN	Mongolia	US	United States of America
FR	France	MR	Mauritania	UZ	Uzbekistan
GA	Gabon			VN	Viet Nam

-1-

METHOD FOR OLEFIN OXIDATION

Field of the Invention

The present invention relates to a process for producing oxidized olefins. More particularly, the invention relates to a process for producing oxidized olefins using a reaction medium containing carbon dioxide.

Background of the Invention

Oxidized olefins such as polyethers, and in particular fluoropolyethers, are employed in numerous applications. In particular, these compounds possess a number of physical properties such as low volatility, high thermal and chemical stability, and low electrical conductivity which makes them suitable for a wide range of end uses. For example, perfluoropolyethers may be utilized in lubricating valves and bearings associated with reactive gas handling; as emulsions in cosmetics; and as defoamers. In addition, the compounds are also desirable for use as treatment agents in protecting the surfaces of buildings and other structures from environmental contaminants.

Fluoropolyethers are manufactured primarily by two techniques, one which involves the ring opening polymerization of cyclic ethers such as hexafluoropropylene oxide and 1,1'-tetrafluorooxetane, and the second which involves the photooxidative polymerization of fluorinated olefins. In general, the

use of photooxidative polymerization is preferred because of the wider range of products that can be prepared from a limited number of polyolefins.

Photooxidative polymerization reactions are often carried out in a liquid solution which contains

-2-

an organic solvent. The range of solvents which may be employed has been known to be limited due to the fact that the fluoroolefins are essentially insoluble in most organics, with the exception of perfluoro and
5 chloro fluorocarbon solvents. The formation of polyethers in these solvents is described in U.S. Patent Nos. 3,442,942; 3,720,646; and 4,451,646 to Sianesi et al; and 5,143,589 and 5,237,108 to Marraccini et al. The utilization of these solvents,
10 however, has been found to become increasingly undesirable due to the expense and heightened environmental risks associated with such. Moreover, when low molecular weight, low boiling polyether compounds are prepared in these solvents, separation of
15 the compounds from the solvents can be difficult, especially when the compounds and solvents display similar properties.

In view of the foregoing, it is an object of the present invention to provide a process for
20 producing oxidized olefins which employs a more cost-effective and environmentally-acceptable reaction medium. Such oxidized olefins may include, for example, fluorinated polyethers and low molecular weight fluorocarbons made from fluoroolefins.

25 It is another object of the present invention to provide a process for making oxidized olefins which allows for easier separation of the oxidized olefins from the reaction medium.

It is a yet a further object of the present
30 invention to provide mixtures of components which may be utilized in the above process.

Summary of the Invention

These and other objects are satisfied by the present invention which includes as a first aspect a
35 process for producing an oxidized olefin. The process comprises providing an olefin and oxygen in combination

-3-

in a reaction medium which comprises carbon dioxide, and oxidizing the olefin in the reaction medium to make the oxidized olefin. Preferably, the oxidizing step is carried out in the presence of ultraviolet light.

- 5 The reaction medium used in the process may comprise supercritical, liquid, or gaseous carbon dioxide. The olefin which is oxidized is preferably a fluoroolefin selected from the group consisting of vinyl fluoride, trifluoroethylene,
- 10 chlorotrifluoroethylene, bromotrifluoroethylene, 1,2-difluoroethylene, $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$; $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$, $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CH}_2\text{OH}$, tetrafluoroethylene, hexafluoropropylene, octafluoroisobutylene,
- 15 perfluorobutene, perfluoropentene, perfluoro(methyl vinyl ether), perfluoro(propyl vinyl ether), perfluoro(2,2-dimethyl-1,3-dioxole), and perfluorocyclobutene.

- The process also provides a step for
- 20 separating the oxidized olefin from the reaction medium subsequent to its formation. In addition, in the embodiment where the oxidized olefin has peroxide linkages, the invention provides a step for decomposing the peroxide linkages from the oxidized olefin to form
- 25 oxidized olefin radicals.

- The present invention includes as a second aspect a mixture of components useful for carrying out the oxidation of an olefin. The mixture comprises an olefin, oxygen, and a reaction medium which comprises
- 30 carbon dioxide. The olefin and oxygen are present in combination in the carbon dioxide.

Detailed Description of the Preferred Embodiments

- The present invention is primarily directed to a process for producing oxidized olefins.
- 35 Specifically, the process comprises providing an olefin and oxygen in combination in a reaction medium which

-4-

comprises carbon dioxide. Subsequently, the olefin becomes oxidized in the reaction medium to form an oxidized olefin. As explained herein, the oxidized olefin may be in form of many end products, including, for example, a fluorinated polyether or a small molecule which results from the oxidation of a fluoroolefin. The process may further comprise the step of separating the oxidized olefin from the reaction medium. The invention also provides a process for producing an oxidized olefin in which an oxidized olefin, a component and a reaction medium is provided and then the component and oxidized olefin react to form an oxidized olefin functionalized with the component. The oxidized olefin of the invention may comprise peroxide linkages. Accordingly, the invention includes a step which decomposes the peroxide linkages from the oxidized olefin.

For the purposes of the invention, carbon dioxide is employed in the reaction medium in a liquid, gaseous, or supercritical phase. If liquid CO₂ is used, the temperature employed during the process is preferably below 31°C. More specifically, liquid CO₂ may be obtained at temperatures from about -55°C to about 31°C and pressures from about 70 psi to 1100 psi. If gaseous CO₂ is used, it is preferred that the phase be employed at high pressure. As used herein, the term "high pressure" generally refers to CO₂ having a pressure from about 20 to about 73 bar. Preferably, the CO₂ is utilized in a "supercritical" phase. As used herein, "supercritical" means that a fluid is at a temperature that is sufficiently high that it cannot be liquified by pressure. The thermodynamic properties of CO₂ are reported in Hyatt, *J. Org. Chem.* **49**: 5097-5101 (1984); therein, it is stated that the critical temperature of CO₂ is about 31°C and the critical pressure is about 1070 psi; thus the method of the present invention should be carried out at a

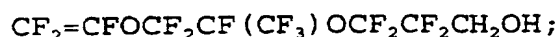
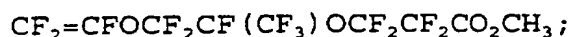
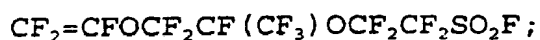
-5-

temperature above 31° and a pressure above 1070 psi. The reaction medium preferably comprises from about 5 to 99 percent by weight of CO₂ based on the weight of the reaction medium, and more preferably from about 50 to 80 percent by weight CO₂.

The reaction medium may also comprise one or more cosolvents along with the CO₂. Illustrative cosolvents include, but are not limited to, perfluorocarbons, hydrofluorocarbons, and perfluoropolyethers. The cosolvent may be added in order to depress the freezing point of the CO₂ which allows the reaction to be carried out at lower temperatures. It is preferred that the cosolvent be substantially inert to reaction with oxygen under the conditions employed in the process of the invention.

Numerous olefins may be employed in the process of the invention and those which are preferred include fluoroolefins. Any suitable fluoroolefins may be employed including those containing functional groups. Suitable functional groups include, for example, esters, sulfonyl fluoride, hydroxyl, or vinyl.

Particularly suitable fluoroolefins may be those with at least one fluorine atom attached to the vinyl moiety and include, but are not limited to vinyl fluoride; trifluoroethylene; chlorotrifluoroethylene; bromotrifluoroethylene; 1,2-difluoroethylene.



$\text{CF}_2=\text{CFOCF}_2\text{CF}_2\text{SO}_2\text{FSF}(\text{CF}_2)_n\text{CH}_2\text{CF}=\text{CF}_2$ where $n=1,2,3,4$, or 5;
 $\text{RCH}_2\text{OCF}=\text{CF}_2$ where R is hydrogen or $\text{F}(\text{CF}_2)_m$ where $m=1, 2$, or

3; and $\text{ROCF}=\text{CH}_2$ where R is $\text{F}(\text{CF}_2)_m$ where m is 1,2,3 or 4.

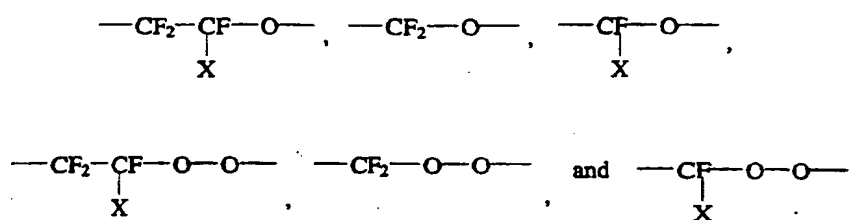
Linear or branched fluorinated olefins having the formula C_nF_{2n} where $n=2-20$ are also suitable and include compounds such as tetrafluoroethylene;

-6-

hexafluoropropylene; octafluoroisobutylene;
perfluorobutene; perfluoropentene; perfluoro(methyl
vinyl ether); perfluoro(ethyl vinyl ether)
perfluoro(propyl vinyl ether); perfluoro(2,2-dimethyl-
5 1,3-dioxole); and perfluorocyclobutene. Preferred
fluorinated olefins are tetrafluoroethylene,
chlorotrifluoroethylene, 2,2-dimethyl-1,3-dioxole,
hexafluoropropylene, perfluoro(methylvinyl ether), and
perfluoro(propyl vinyl ether). Combinations of
10 fluorinated olefins may be employed when it is desired
to produce polyethers in the form of copolymers.
Suitable combinations include
hexafluoropropylene/tetrafluoroethylene, as well as
those utilizing perfluoro(propyl vinyl ether),
15 $\text{CF}_2=\text{FOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$, $\text{CF}_2=\text{C}$
 $\text{FOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$, tetrafluoroethylene, and
hexafluoropropylene. The olefins are preferably
employed in an amount ranging from about 1 to 95
percent based on the weight of the reaction medium and
20 more preferably, from about 5 to 50 percent by weight.

A wide number of known and suitable oxidized
olefins may be made by the present invention. In one
embodiment, polyethers can be produced, more preferably
fluoropolyethers, and most preferably
25 perfluoropolyethers. In another embodiment, low
molecular weight molecules may be produced from the
oxidation process, which preferably includes those
which comprise fluorine, oxygen, and carbon. In
general, the preferred structure of the
30 perfluoropolyethers will have a backbone comprised
mainly of the units:

- 7 -



wherein X is fluorine, trifluoromethyl, or suitable other fluoroalkyl or fluoroether groups. As is known by those skilled in the art, the exact distribution of these structures obtained in the fluorinated polyether will be a function of reaction conditions including the viscosity of the reaction medium. The viscosity of the solvent will influence effects which play an important role in radical recombination reactions. End groups which may be present on the perfluoropolyether include acid fluoride, formyl fluoride, or other fluoroalkyl species. The perfluoropolyethers may also contain a group which imparts functionality to the polymer. In particular, such a group may be located at the end of the polymer chain, or on random sites along the chain.

Low molecular weight compounds may include, for example, the oxidation products of hexafluoropropylene such as trifluoroacetyl fluoride, carbonyl fluoride, hexafluoropropylene oxide, and the like. Low molecular weight compounds derived from other components such as tetrafluoroethylene may also be produced.

For the purposes of the invention, functionality may be imparted to the oxidized olefin by oxidizing an olefin which contains functionality, or by reacting the oxidized olefin with a suitable component to form an oxidized olefin functionalized with the component. Suitable components include monomers and

- 8 -

chain transfer agents. Functionality may also be imparted to the oxidized olefin by removing peroxide linkages from the oxidized olefin by reacting the oxidized olefin with a suitable reagent, described in greater detail herein. Exemplary monomers which may be utilized include, but are not limited to,

5 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$,
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$,
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CH}_2\text{OH}$, and $\text{CF}_2=\text{CF}(\text{CF}_3)\text{Cl}$. Other

10 monomers which may be used contain functional groups such as, for example, acid fluoride, epoxy, amide, cyano, alcohol, and amine. As a specific example, perfluorobutadiene may be used in which one double bond undergoes photooxidative polymerization and the other

15 bond is oxidized to a functional group, such as an epoxide, in the oxidized olefin. Suitable chain transfer agents include compounds, for example, which contain a halogen group such as chlorine, bromine, or iodine.

20 The process of the present invention is preferably carried out in the presence of light, preferably ultraviolet light. As known, the actual wavelength and distribution of wavelengths employed as well as the intensity of the light can effect oxidized

25 olefin yield, as well as its molecular weight and chemical composition such as peroxide content and carbon-to-oxygen ratio. Accordingly, those skilled in the art will appreciate that manipulation of the light source can be used to optimize yields under various

30 conditions to favor formation of one type of oxidized olefin over another. Ultraviolet light is preferably employed having a wavelength from 180 nm to 500 nm.

The process of forming an oxidized olefin can be carried out using apparatus and conditions known to those skilled in the art. As an example, the process

35 may be carried out in batch, semi-batch or continuous modes in an appropriate reaction vessel, preferably one

-9-

that may withstand high pressures. A suitable high pressure reaction vessel may employ various means and features to facilitate the formation of the oxidized olefins. For example, the vessel may use heating means
5 such as an electric furnace to bring the reaction to the desired temperature. Mixing means can also be used in the reaction vessel and include stirrers such as paddle stirrers, impeller stirrers, blades, and the like.

10 In particular, the process of forming an oxidized olefin usually begins by feeding a mixture of olefin and carbon dioxide into the reaction vessel. In a usual instance, the carbon dioxide constitutes the reaction medium in which the process is carried out
15 although other components may be present. The vessel is then closed and is brought to the desired temperature and pressure. The reaction is preferably carried out at a temperature from about -80°C to about 200°C , and more preferably, from about -60°C to about
20 80°C . The pressure employed during the reaction preferably ranges from about 15 psi to about 20,000 psi, and more preferably from about 50 psi to about 5,000 psi. Oxygen is then supplied to the reaction mixture. In general, the oxygen may be added to the
25 reaction vessel all at once or may be added continuously by bubbling it through the olefin and carbon dioxide in the event that liquid carbon dioxide is employed. A positive pressure of oxygen may be maintained in the vessel if desired, so as to replenish
30 the oxygen which is consumed in the reaction. For the purposes of the invention, the oxygen may be added in its pure molecular form or may be diluted with an inert diluent such as nitrogen to reduce the potential for an explosion. During addition of the oxygen, the mixture
35 is preferably irradiated with light to promote the carrying out of the reaction. The reaction proceeds until the desired yield of oxidized olefin is obtained.

-10-

In an alternative embodiment, the oxygen and olefin may be added simultaneously to the reactor. As an example, the two components may be added continuously in the event that a continuous or a semi-
5 batch reaction mode is utilized.

As is known, oxidized olefin compounds, and in particular perfluoropolyethers, often comprise excess peroxide linkages. It is often desirable to remove the excess peroxide linkages in order to add
10 stability to the compound. The present invention provides a process step in which the peroxide linkages are decomposed from these compounds which may be carried out, for example, by chemical, photochemical, or thermal means. The method of peroxide removal must
15 be compatible in carbon dioxide, with the peroxide removal being accomplished directly in the carbon dioxide, either in-situ or as a separate step subsequent to the formation of the oxidized olefin. Chemically, the peroxide linkages may be removed by
20 reacting the oxidized olefins with reagents including appropriate bases such as amines, hydroxide, fluorine, and bromine. Photochemically, the linkages may be removed by employing a suitable compound such as a quinone in conjunction with ultraviolet light,
25 preferably of a wavelength between 240 nm and 400 nm.

In removing the peroxide linkages from the oxidized olefins, oxidized olefin free radicals are formed which are capable of reacting with numerous types of compounds so as to form a variety of products.
30 For example, as is known, reacting the oxidized olefins with a reagent such as a suitable base or fluoride at elevated temperatures, or bromine, yields an oxidized olefin (e.g., a perfluoropolyether) which is functionalized at the end of the polymer chain. For
35 example, a perfluoropolyether having bromine-containing end groups may be formed. Additionally, removal of oxidized olefin (e.g., perfluoropolyether) peroxide

-11-

linkages using either a thermal method or ultraviolet light in combination with a quinone compound results in the formation of an oxidized olefin bridged by the quinone. As is known, the resulting oxidized olefin is capable of undergoing subsequent free radical polymerization with a suitable monomer such as a vinyl monomer, which is capable of leading to the formation of functional copolymers such as block or blocky copolymers. In addition, a suitable polymer may be provided and the oxidized olefin radicals may be grafted onto the polymer.

An advantage afforded by a reaction medium which comprises carbon dioxide is the high solubility of hydrocarbon-based monomers relative to many fluorinated solvents, including fluorinated polyether-based solvents, which will allow for the synthesis of new materials not possible in fluorinated solvents.

Subsequent to the formation of any of the oxidized olefin compounds referred to herein, the present invention further provides a step for separating the oxidized olefin from the reaction medium. Any of the known and suitable techniques may be employed to carry out this process step. For example, the oxidized olefin may be separated from the reaction medium by venting the reaction medium to the atmosphere or to a recycle stream. Additionally, the oxidized olefin may be extracted and transferred with the carbon dioxide to another vessel. Subsequently, the carbon dioxide is expanded to lower pressure and is allowed to escape, which causes the oxidized olefin to separate from the carbon dioxide.

In the event that multiple compounds are formed in the oxidation reaction, any of the suitable techniques may be employed to separate the compounds. For example, pressure and temperature profiling techniques may be used in all reaction modes.

-12-

Specifically, the profiling may be done continuously or, in the case of a batch mode, may be accomplished by extracting the compounds by employing different pressures and temperatures throughout the reaction.

5 The oxidized olefins produced in accordance with the invention may be employed in a wide variety of end uses. Perfluoropolyethers, for example, can be used as lubricants which possess adequate physical
10 and temperature conditions; thermal shock fluids; and as heat transfer/cooling media. Functional polyethers, and more specifically functional perfluoropolyethers, may be used as cosmetics, in emulsion applications, and as coatings such as those used in protecting exposed
15 surfaces such as stone. Low molecular weight compounds are useful when employed in a number of chemical syntheses. For example, hexafluoropropylene oxide is useful in the preparation of fluoroalkyl vinyl ester monomers such as perfluoro (propyl vinyl ether),
20 perfluoro (methyl vinyl ether). Additionally, carbonyl fluoride is useful in the preparation of perfluoro (methyl vinyl ether).

The present invention is explained in greater detail herein in the following examples, which are
25 illustrative and are not to be construed as limiting of the invention. In the following examples, "psi" means pounds per square inch, and ^{19}F NMR means fluorine nuclear magnetic resonance spectroscopy.

Example 1

30 **Photooxidation of Hexafluoropropylene**

A 25-mL high pressure reactor, with a sapphire window to allow the introduction of light, is maintained at a temperature of approximately -10°C . 10 grams hexafluoropropylene is condensed into the reactor
35 at high pressure, 11 grams liquid carbon dioxide is added, and the cell is charged with molecular oxygen to

-13-

approximately 2000 psi. The cell is then subjected to irradiation through the sapphire window using a 140 watt mercury arc lamp (Hanovia model 616A-13) for 24 hours. The reactor is then pressurized to 2500 psi with carbon dioxide and extracted with three reactor volumes into a cold trap maintained at -78°C , thus allowing the carbon dioxide to escape into the atmosphere. 0.5 grams of clear, viscous, fluid is then collected in the cold trap, corresponding to a 5% yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

Example 2

Photooxidation of Hexafluoropropylene

The reactor described in Example 1 is employed under the conditions described except that 9.9 grams hexafluoropropylene and 12 grams liquid carbon dioxide is used. Additionally, the reactor is maintained at a temperature of 0°C . 0.5 grams of clear, viscous, fluid is collected in the cold trap. Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

Example 3

Photooxidation of Hexafluoropropylene

The procedure described in Example 1 is employed in which 9.8 grams of hexafluoropropylene is condensed and 12 grams of carbon dioxide is used. The temperature of the reactor is maintained at 20°C and 0.4 grams of clear, viscous fluid is collected in the cold trap corresponding to a 4% yield. Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

-14-

Example 4**Photooxidation of Hexafluoropropylene**

The procedure described in Example 1 is employed in which 10.1 grams hexafluoropropylene is condensed, 12 grams liquid carbon dioxide is added, and the cell is charged with 600 psi molecular oxygen. The cell is then subjected to irradiation for 6 hours. 2.2 grams of clear, viscous, fluid is collected in the cold trap corresponding to a 22% yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

Example 5**Photooxidation of Hexafluoropropylene**

The procedure described in Example 4 is employed in which 7.9 grams of hexafluoropropylene is condensed and 12.1 grams liquid carbon dioxide is added to the reactor. 1.9 grams of a clear, viscous, fluid is collected in the cold trap corresponding to a 24% yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

Example 6**Photooxidation of Perfluoro(propyl vinyl ether)**

The procedure described in Example 4 is employed in which 10.7 grams of perfluoro (propyl vinyl ether) is condensed, 12 grams liquid carbon dioxide is added, and the cell is subjected to irradiation for 24 hours. 2.1 grams of a clear, viscous, fluid is collected in the cold trap corresponding to a 19% yield of perfluoropolyether [based on perfluoro (propyl vinyl ether)]. Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

-15-

Example 7**Photooxidation of EVE ($\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$)**

- The procedure described in Example 6 is employed in which 12 grams ester vinyl ether
- 5 ($\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$) is added to the reactor via syringe and 12 grams liquid carbon dioxide is also added. 11.2 grams of a clear fluid is collected in the cold trap corresponding to a 95% yield of perfluoropolyether (based on hexafluoropropylene).
- 10 Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether structure.

Example 8**Photooxidation of Hexafluoropropylene**

- The procedure described in Example 1 is
- 15 employed with the reactor being maintained at a temperature of approximately -5°C . 11.2 grams hexafluoropropylene is condensed in at high pressure, 11.5 grams liquid carbon dioxide is added, and the cell is subject to irradiation using a 450 watt mercury arc
- 20 lamp (Hanovia Model 679A36). 5.5 grams of a clear, fluid is collected in the cold trap corresponding to a 49% yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR spectroscopy is consistent with a perfluoropolyether
- 25 structure.

Example 9**Photooxidation of Hexafluoropropylene**

- The procedure described in Example 8 is employed in which 10.6 grams of hexafluoropropylene is
- 30 condensed in at high pressure, and 13 grams liquid carbon dioxide is added. The temperature is raised to 20°C prior to the cell being charged with oxygen. 7.1 grams of a clear, fluid is collected in the cold trap corresponding to a 70% yield of perfluoropolyether
- 35 (based on hexafluoropropylene). Analysis using ^{19}F NMR

-16-

spectroscopy is consistent with a perfluoropolyether structure.

Example 10

Photooxidation of Hexafluoropropylene

5 The procedure described in Example 9 is employed in which 10.2 grams hexafluoropropylene is condensed in at high pressure and 12 grams liquid carbon dioxide is added. The temperature is raised to 60°C, and the cell is charged with molecular oxygen to
10 approximately 2,500 psi. Oxygen is supplied continuously to the reactor. 0.5 grams of a clear fluid is collected in the cold trap corresponding to a 5 % yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR
15 spectroscopy is consistent with a perfluoropolyether structure. Analysis of portions of the gaseous products shows evidence of carbonyl fluoride and trifluoroacetyl fluoride in addition to other low molar mass fluorooxy compounds.

20

Example 11

Co-photooxidation of Tetrafluoroethylene and Hexafluoropropylene

 The procedure described in Example 10 is employed with the temperature being maintained at
25 approximately -10 °C. 6.0 grams hexafluoropropylene is condensed in at high pressure, followed by the addition of 10 grams of a 50/50 wt/wt mixture of tetrafluoroethylene (5 g) and carbon dioxide (5g). 6 grams of additional liquid carbon dioxide is added to
30 the reactor, and the cell is charged with molecular oxygen to approximately 1,500 psi. 5.0 grams of a clear, fluid is collected in the cold trap corresponding to a 45 % yield of perfluoropolyether (based on hexafluoropropylene). Analysis using ^{19}F NMR

-17-

spectroscopy is consistent with a perfluoropolyether structure.

Example 12

Thermal Oxidation of Hexafluoropropylene

5 The reactor described in Example 1 is employed with 10 grams of hexafluoropropylene and 10 grams of CO₂, except that the temperature employed in 100°C and the oxidation is carried out in the absence of UV light.

Example 13

Thermal Oxidation of Tetrafluoroethylene

10 The reactor described in Example 1 is employed with 10 grams of tetrafluoroethylene and 10 grams of CO₂, except that the temperature employed is 15 100°C and the oxidation is carried out in the absence of UV light.

Example 14

Photochemical removal of peroxide linkages

A perfluoropolyether is prepared according to 20 any of the above examples which has peroxide linkages. The perfluoropolyether is subjected to further irradiation in a reaction medium comprising carbon dioxide to remove the peroxide linkages.

Example 15

Thermal removal of peroxide linkages

25 A perfluoropolyether is prepared according to any of the above examples which has peroxide linkages. The perfluoropolyether is subjected to heating in a reaction medium comprising carbon dioxide to remove the 30 peroxide linkages.

-18-

Example 16**Removal of peroxide linkages using bromine**

- A perfluoropolyether is prepared according to any of the above examples which has peroxide linkages.
- 5 The perfluoropolyether is subjected to reaction with bromine in a reaction medium comprising carbon dioxide to remove the peroxide linkages, and impart bromine-containing end groups to the compound.

Example 17

- 10 **Decomposition of Perfluoropolyether Peroxide in the Presence of a Functionalization Reagent**

- A perfluoropolyether is prepared according to any of the above examples which has peroxide linkages. The linkages are decomposed in the presence of a
- 15 reagent capable of reacting with the fluoroalkyl alkoxy radicals to yield end functional perfluoropolyethers.

Example 18**Decomposition of Perfluoropolyether Peroxide in the Presence of a Vinyl Monomer**

- 20 A perfluoropolyether is prepared according to any of the above examples which has peroxide linkages. The linkages are decomposed in the presence of a vinyl monomer capable of reacting with the fluoroalkyl alkoxy radicals to yield a copolymer.

25

Example 19**Grafting of Perfluoropolyethers**

- A perfluoropolyether is prepared according to any of the above examples which has peroxide linkages. The linkages are decomposed in the presence of a
- 30 polymer capable of undergoing grafting reactions with the fluoroalkyl alkoxy radicals to yield a copolymer.

-19-

The foregoing examples are illustrative of the present invention, and are not to be construed as limiting thereof. The invention is defined by the following claims, with equivalents of the claims to be
5 included therein.

-20-

THAT WHICH IS CLAIMED:

1. A process for preparing an oxidized olefin comprising:
providing an olefin and oxygen in combination
5 in a reaction medium which comprises carbon dioxide;
and
oxidizing the olefin in the reaction medium
to make the oxidized olefin.
2. The process according to Claim 1 wherein
10 said oxidizing step is carried out in the presence of
ultraviolet light.
3. The process according to Claim 1 wherein
the reaction medium comprises supercritical carbon
dioxide.
- 15 4. The process according to Claim 1 wherein
the reaction medium comprises liquid carbon dioxide.
5. The process according to Claim 1 wherein
the reaction medium comprises gaseous carbon dioxide.
6. The process according to Claim 1 wherein
20 the olefin is a fluoroolefin.
7. The process according to Claim 6 wherein
the fluoroolefin is selected from the group consisting
of vinyl fluoride, trifluoroethylene,
chlorotrifluoroethylene, bromotrifluoroethylene, 1,2-
25 difluoroethylene, $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$;
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$,
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CH}_2\text{OH}$, tetrafluoroethylene,
hexafluoropropylene, octafluoroisobutylene,
perfluorobutene, perfluoropentene, perfluoro(methyl
30 vinyl ether), perfluoro(propyl vinyl ether),

-21-

perfluoro(ethyl vinyl ether), perfluoro(2,2-dimethyl- 1,3-dioxole), and perfluorocyclobutene.

8. The process according to Claim 1 wherein the oxidized olefin is selected from the group
5 consisting of carbonyl fluoride, trifluoroacetyl fluoride, tetrafluoroethylene oxide, and hexafluoropropylene oxide.

9. The process according to Claim 1 wherein the oxidized olefin is a polyether.

10 10. The process according to Claim 1 wherein the oxidized olefin has peroxide linkages.

11. An oxidized olefin prepared according to the process of Claim 1, wherein said oxidized olefin is a polyether.

15 12. A process for preparing an oxidized olefin comprising:

providing an olefin and oxygen in combination in a reaction medium comprising carbon dioxide;

20 oxidizing the olefin in the reaction medium to make the oxidized olefin; and

separating the oxidized olefin from the reaction medium.

13. The process according to Claim 12
25 wherein said oxidizing step is carried out in the presence of ultraviolet light.

14. The process according to Claim 12 wherein the reaction medium comprises supercritical carbon dioxide.

-22-

15. The process according to Claim 12 wherein the reaction medium comprises liquid carbon dioxide.

16. The process according to Claim 12
5 wherein the reaction medium comprises gaseous carbon dioxide.

17. The process according to Claim 12 wherein the olefin is a fluoroolefin.

18. The process according to Claim 17
10 wherein the fluoroolefin is selected from the group consisting of vinyl fluoride, trifluoroethylene, chlorotrifluoroethylene, bromotrifluoroethylene, 1,2-difluoroethylene, $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$;
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$,
15 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CH}_2\text{OH}$, tetrafluoroethylene, hexafluoropropylene, octafluoroisobutylene, perfluorobutene, perfluoropentene, perfluoro(methyl vinyl ether), perfluoro(ethyl vinyl ether), perfluoro(propyl vinyl ether), perfluoro(2,2-dimethyl-
20 1,3-dioxole), and perfluorocyclobutene.

19. The process according to Claim 12 wherein the oxidized olefin is selected from the group consisting of carbonyl fluoride, trifluoroacetyl fluoride, tetrafluoroethylene oxide, and
25 hexafluoropropylene oxide.

20. The process according to Claim 12 wherein the oxidized olefin is a polyether.

21. The process according to Claim 12 wherein the polyether has peroxide linkages.

-23-

22. An oxidized olefin prepared according to the process of Claim 12, wherein said oxidized olefin is a polyether.

23. A process for preparing an oxidized
5 olefin comprising:

providing an oxidized olefin and a component in combination in a reaction medium comprising carbon dioxide; and

10 reacting the component with the oxidized olefin to make an oxidized olefin functionalized with the component.

24. The process according to Claim 23 wherein the reaction medium comprises supercritical carbon dioxide.

15 25. The process according to Claim 23 wherein the reaction medium comprises liquid carbon dioxide.

26. The process according to Claim 23 wherein the reaction medium comprises gaseous carbon
20 dioxide.

27. The process according to Claim 23 wherein the oxidized olefin is selected from the group consisting of carbonyl fluoride, trifluoroacetyl fluoride, tetrafluoroethylene oxide, and
25 hexafluoropropylene oxide.

28. The process according to Claim 23 wherein the oxidized olefin is a polyether.

-24-

29. The process according to Claim 23 wherein the component is selected from the group consisting of monomers, chain transfer agents, and reagents.

5 30. An oxidized olefin prepared by the process of Claim 23, wherein said oxidized olefin is a polyether.

 31. A process for removing peroxide linkages from an oxidized olefin comprising:
10 providing the oxidized olefin having peroxide linkages in a reaction medium which comprises carbon dioxide; and
 decomposing the peroxide linkages from the oxidized olefin to form an oxidized olefin radical.

15 32. The process according to Claim 31 wherein the oxidized olefin is a perfluoropolyether.

 33. The process according to Claim 31 wherein said decomposing step is performed thermally.

 34. The process according to Claim 31
20 wherein said decomposing step is performed photochemically.

 35. The process according to Claim 31 wherein said decomposing step is performed chemically.

 36. The process according to Claim 31
25 wherein the reaction medium further comprises a reagent capable of reacting with the oxidized olefin radical.

-25-

37. The process according to Claim 31 wherein the reaction medium further comprises a vinyl monomer, and wherein the oxidized olefin radical reacts with the vinyl monomer during said decomposing step to
5 form a copolymer.

38. The process according to Claim 31 wherein the reaction medium further comprises a polymer, and wherein the oxidized olefin radical is grafted onto the polymer during said decomposing step.

10 39. A mixture of components suitable for carrying out the oxidation of an olefin, said mixture comprising an olefin, oxygen and a reaction medium which comprises carbon dioxide, said olefin and said oxygen being present in combination in said reaction
15 medium.

40. The mixture of components according to Claim 39 wherein said reaction medium comprises supercritical carbon dioxide.

41. The mixture of components according to
20 Claim 39 wherein said reaction medium comprises liquid carbon dioxide.

42. The mixture of components according to Claim 39 wherein said reaction medium comprises gaseous carbon dioxide.

25 43. The mixture of components according to Claim 39 wherein said olefin is a fluoroolefin.

-26-

44. The mixture of components according to Claim 43 wherein the fluoroolefin is selected from the group consisting of vinyl fluoride, trifluoroethylene, chlorotrifluoroethylene, bromotrifluoroethylene, 1,2-
5 difluoroethylene, $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{SO}_2\text{F}$;
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CO}_2\text{CH}_3$,
 $\text{CF}_2=\text{CFOCF}_2\text{CF}(\text{CF}_3)\text{OCF}_2\text{CF}_2\text{CH}_2\text{OH}$, tetrafluoroethylene,
hexafluoropropylene, octafluoroisobutylene,
perfluorobutene, perfluoropentene, perfluoro(methyl
10 vinyl ether), perfluoro(ethyl vinyl ether)
perfluoro(propyl vinyl ether), perfluoro(2,2-dimethyl-
1,3-dioxole), and perfluorocyclobutene.

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US97/01518

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) : Please See Extra Sheet.

US CL : Please See Extra Sheet.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 522/83, 181, 184, 185, 186, 187, 189; 526/235, 247, 250, 252, 253, 255, 335, 336, 337, 338, 348.6, 348.7, 351, 352, 352.2.

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

APS: OLEFIN, FLUOROLEFIN, PERFLUOROMETHYL VINYL ETHER, CARBON DIOXIDE, SUPERCRITICAL, LIQUID, GASEOUS, OXYGEN, OXIDIZE, RADIATION, ULTRAVIOLET.

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 3,522,228 A (FUKUI ET AL) 28 July 1970, column 1, lines 18-22 and 57-69, column 2, lines 5-19, column 2, line 68, to column 3, line 20.	1-44
Y	US 5,236,602 A (JACKSON) 17 August 1993, Abstract, column 4, lines 46-68, column 5, lines 27-35, column 6 to column 7, line 15, column 8, lines 64-67.	1-44
Y	US 5,237,108 A (MARRACCINI ET AL) 17 August 1993, Abstract, column 4, lines 40-66, column 9, lines 18-30, Examples 1A and 1B.	1-44
Y	GB 1,097,679 A (SOCIETA EDISON S.p.A.) 03 January 1968, page 1, lines 13-30.	1-44



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:	*T later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
A document defining the general state of the art which is not considered to be of particular relevance	*X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
E earlier document published on or after the international filing date	*Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
L document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	*G* document member of the same patent family
O document referring to an oral disclosure, use, exhibition or other means	
P document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

04 APRIL 1997

Date of mailing of the international search report

14 APR 1997

Name and mailing address of the ISA/US
Commissioner of Patents and Trademarks
Box PCT
Washington, D.C. 20231

Facsimile No. (703) 305-3230

Authorized officer

SUSAN BERMAN

Telephone No. (703) 308-1235

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US97/01518

C (Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 3,442,942 A (SIANESI ET AL) 06 May 1969, Abstract, column 2, line 51, to column 3, line 7, column 4, lines 35-39, column 9, line 39, to column 10, line 2.	1-44
Y	US 4,451,646 A (SIANESI ET AL) 29 May 1984, Abstract and examples.	1-44
Y	US 5,104,911 A (MARCHIONNI ET AL) 14 April 1992, column 1, lines 31-49, column 2, lines 38-60, column 3, lines 15-32, Example 1 and claim 3.	1-44
Y	CA 0,611,156 A (SHELL OIL COMPANY) 20 December 1960, column 1, lines 16-23, 35-45, column 2, lines 36-55.	1-44
Y	US 5,386,055 A (LEE ET AL) 31 January 1995, Abstract, column 1, line 44, to column 2, line 4, column 4, line 40, to column 5, line 66.	1-44
Y	US 4,970,093 A (SIEVERS ET AL) 13 November 1990, Abstract, column 2, lines 15-42, column 3 and Table 1, column 5, lines 16-21, column 6, lines 3-49.	1-44
Y	US 5,143,589 A (MARCHIONNI ET AL) 01 September 1992, Abstract, column 3, lines 29-54.	1-44
Y	US 3,720,646 A (SIANESI ET AL) 13 March 1973, Abstract.	1-44

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US97/01518

Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This international report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:

2. ☐ Claims Nos.:
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:

3. ☐ Claims Nos.:
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

Please See Extra Sheet.

1. ☒ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:

4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

☐
☐

The additional search fees were accompanied by the applicant's protest.

No protest accompanied the payment of additional search fees.

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US97/01518

A. CLASSIFICATION OF SUBJECT MATTER:

IPC (6):

C08G 67/00, 85/00; C08J 3/28; C08F 2/48, 4/28, 10/00, 10/02, 10/04/, 10/06, 10/08, 10/10, 10/14, 14/18, 14/24, 14/26, 14/28.

A. CLASSIFICATION OF SUBJECT MATTER:

US CL :

522/83, 181, 184, 185, 186, 187, 189; 526/235, 247, 250, 252, 253, 255, 335, 336, 337, 338, 348.6, 348.7, 351, 352, 352.2.

BOX II. OBSERVATIONS WHERE UNITY OF INVENTION WAS LACKING

This ISA found multiple inventions as follows:

This application contains the following inventions or groups of inventions which are not so linked as to form a single inventive concept under PCT Rule 13.1. In order for all inventions to be searched, the appropriate additional search fees must be paid.

Group I, claim(s) 1-11, drawn to a process for preparing oxidized olefin and the product prepared.

Group II, claim(s) 12-21, drawn to a second process for preparing an oxidized olefin.

Group III, claim(s) 22, drawn to the product prepared by the process of claim 12.

Group IV, claim(s) 23-29, drawn to a third process for preparing a "functionalized" oxidized olefin.

Group V, claim(s) 30, drawn to the product prepared by the process of claim 23.

Group VI, claim(s) 31-38, drawn to a process for removing peroxide linkages from an oxidized olefin.

Group VII, claim(s) 39-44, drawn to a composition.

The inventions listed as Groups I-VII do not relate to a single inventive concept under PCT Rule 13.1 because, under PCT Rule 13.2, they lack the same or corresponding special technical features for the following reasons: (1) with regard to the processes of Groups I-V, there is no evidence of record to show that providing an olefin and oxygen in a reaction medium which comprises carbon dioxide, which is a feature of each process, is a special technical feature. (2) With regard to Group VI, the claims do not require that the oxidized olefin which is to be treated have been prepared by the processes set forth in any of Groups I-VI. 93) With regard to the composition of Group VII, there is no evidence that the particular combination set forth is a special technical feature shared with Groups I-VI which provides unexpected results compared with the prior art. Oxidized olefins and methods for their preparation are known in the art. Oxygen is known as an oxidizing agent in such processes. Solvents are routinely employed in such processes. There is no comparative evidence of record to show that carbon dioxide as solvent or as a component of air containing oxygen provides a special technical feature.